

# Transport of oil in pipelines with core-annular flow

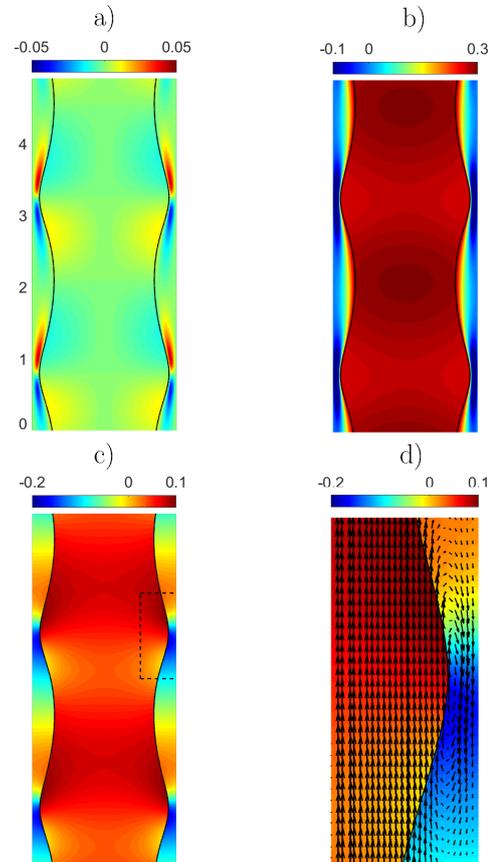
## Flow transitions and regimes in core-annular pipe flow

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### In Short

- Core-Annular pipe flow has applications in transporting highly viscous fluid
- The core-annular flow is unstable to perturbations and can exhibit multiple flow configurations
- Bamboo waves flow configuration allows efficient transport of heavy oil, while slugging deteriorates the efficiency
- Goal: Investigate the flow transitions and the underlying bifurcation mechanism

In Core-annular flow, one type of fluid flows in the core area of a pipe and another type of fluid flows in the annulus near the pipe wall, surrounding the core flow. One of the applications of this flow in industry is the transport of highly viscous crude oil using water, which is hundreds of times less viscous than the crude, in the annulus near to pipe wall to reduce the friction drag. This strategy can greatly reduce the pumping energy cost compared to pumping pure oil in pipelines. Although perfect core annular flow is an ideal flow configuration for this purpose, it is in general linearly unstable [1]-[3], the flow configuration can not be kept because even infinitesimal perturbations suffice to significantly disturb the flow and to change the flow configuration. Depending on the operating condition, the destabilised flow can exhibit various configurations ranging from annular flow (such as the bamboo-shaped waves shown in figure 1), slug flows (the core flow appears as elongated slugs isolated by the other fluid), bubble flow, and droplets dispersed in the other fluid (a more detailed description of the different flow configurations can be found in [1]), and fully stratified flows in horizontal pipes if the two fluids have different density [1]. Different flow configurations are accompanied by different driving pressure gradient (pumping energy cost) and different oil transport efficiency. As the perfect core-annular flow usually cannot be maintained, the annular flow (bamboo waves, short bamboo waves and disturbed core-annular flow) allows the most efficient transport. However, the slugging will significantly deteriorate the efficiency and further lead the flow to bubble flow and dispersion flow. It is of both physical and practical importance to study the slugging process and the underlying bifurcation on the boundary between the annular flow and the slug flow regimes.



**Figure 1:** Axisymmetric bamboo wave flow configuration in CAF with large viscosity ratio. The bold black line shows the position of the interface between oil and water [7]. (a) Radial velocity. (b) axial velocity. (c) Fluid pressure. (d) In-plane velocity field (vectors) and fluid pressure (colormap), close to the wave crest in the small region enclosed by the window defined by dashed lines in panel (c).

Up to now there are very limited studies on this problem, especially theoretical studies. They are only limited to linear stability analysis of perfect core-annular flow [[2],[3]] and cannot shed light on more complex flow configurations and nonlinear regimes. The experimental studies of Ref. [1] and [4] gave some phase diagrams for water-oil system for vertical up-flow, vertical down-flow, and horizontal pipe system. Although the diagrams gave a description of the rich flow regimes, they are rather crude and the boundaries between different flow regimes (configurations) were not clearly determined. Therefore, the flow states very close to the boundaries are still unknown. Besides, the bifurcation leading to different flow regimes and the sensitivity of the phase-diagram on the initial condition has not been investigated. Hence, more accu-

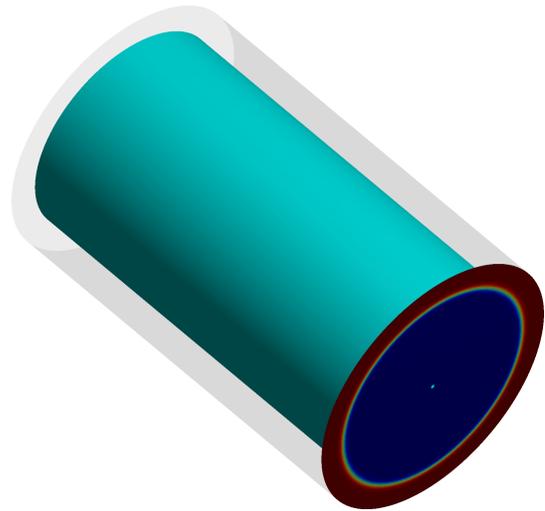
rate studies of the phase diagram in non-dimensional parameter space, and especially the transition mechanism between different regimes are highly desired for a better understanding of the rich dynamics of the core-annular flow and for general applications. The aim of this project is to investigate this problem using numerical simulation. The challenge to numerical simulation of multi-phase flows generally comes in two aspects: 1) to correctly capture the interfacial tension force, and 2) to correctly capture the interface topological changes such as the breaking of annular flow into slugs or merging of slugs into annular flows. To address these challenge, a good candidate is the phase-field method, which is thermodynamically consistent and can naturally capture the motion of the interface between different phases or fluids [5]. We developed a highly efficient in-house code using high-order finite difference and spectral method for discretisation and using phase field method to simulate binary flow systems. The code is parallelised using MPI+OpenMP and this allows to efficiently utilise up to  $O(10^4)$  CPU cores [6]. It has been validated in various flows. Especially, we have successfully obtained the bamboo wave flow regime using our numerical tool in heavily oil-water system and got quantitative agreement with former studies in both the nonlinear regime and the linear regime that leads to the final bamboo wave [7]. Note that the very high viscosity ratio between heavy oil and water is a challenge for the phase-field method. Besides, in our method, non-dimensional parameters such as Reynolds number for each fluid (defined by the nominal flow rate of each fluid), viscosity ratio, density ratio, and surface tension (capillary number) etc. can be easily controlled for probing the boundaries between regimes and for determining the most relevant parameter in the transition from one regime to another. Moreover, we expanded our research to cover flow regimes at higher Re, such as the transition to turbulence of CAF at moderate Reynolds (Re = 3000-12000 and the breakage of slugs and drops in turbulent flow. See figures 2 and 3 for an example of the transition from laminar CAF to turbulent stratified flow at Re = 3000.

## WWW

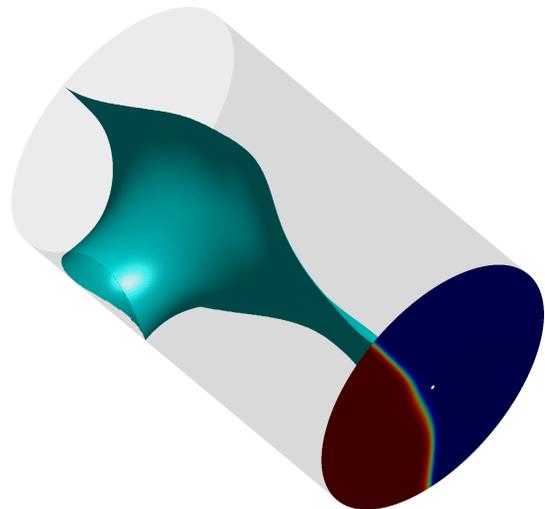
<https://www.zarm.uni-bremen.de/>

## More Information

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**Figure 2:** Interface, initial state CAF, Re = 3000



**Figure 3:** Interface, saturated state, CAF, Re = 3000

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